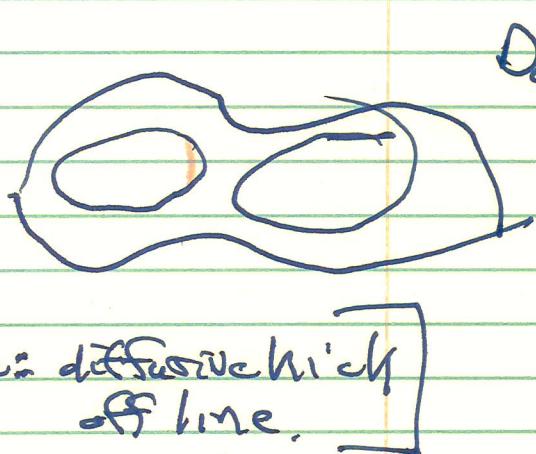


Notes 5 - Collisional Diffusion = Scattering

→ Taylor Cells

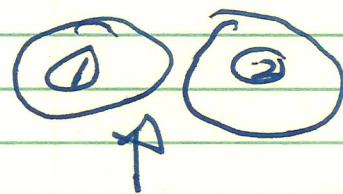
→ Taylor Shear Dispersion

→ Recall 2-D front part of stochastic field



$D_0 \neq 0!$

, E cells close



collisional diffusion
can kick $\textcircled{1} \rightarrow \textcircled{2}$

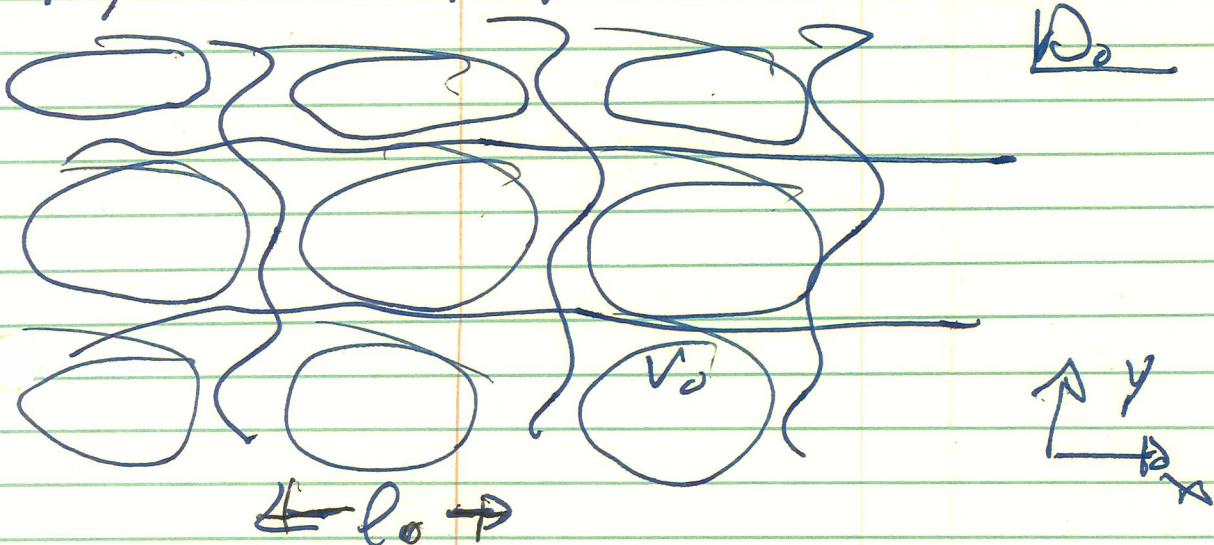
$$D_{\perp \text{ eff}} = D_{\perp} (\tilde{b}, \Delta_{\perp}, D_0)$$

↓ corresponds to D_m here

→ Many problems involve synergy between turbulent scattering and collisional diffusion

→ Taylor Problem - the classic

Geometry matters



2. 6. 1

For periodic scalar problem:

$$\frac{\partial n}{\partial t} + \underline{v} \cdot \underline{\nabla} n - D_s \nabla^2 n = 0$$

can define: $\lambda_e = V_0 l_0 / D_s$
 → Peclet number
 → Pe>>1 of interest

Interest :- Effect transport coefficient, i.e.
 diffusivity for scales $L \gg l_0$

* - effective medium problem with
 2 transport processes:

fast \rightarrow convection \rightarrow operating in cells
 slow \rightarrow diffusion \rightarrow operating in boundary layers.

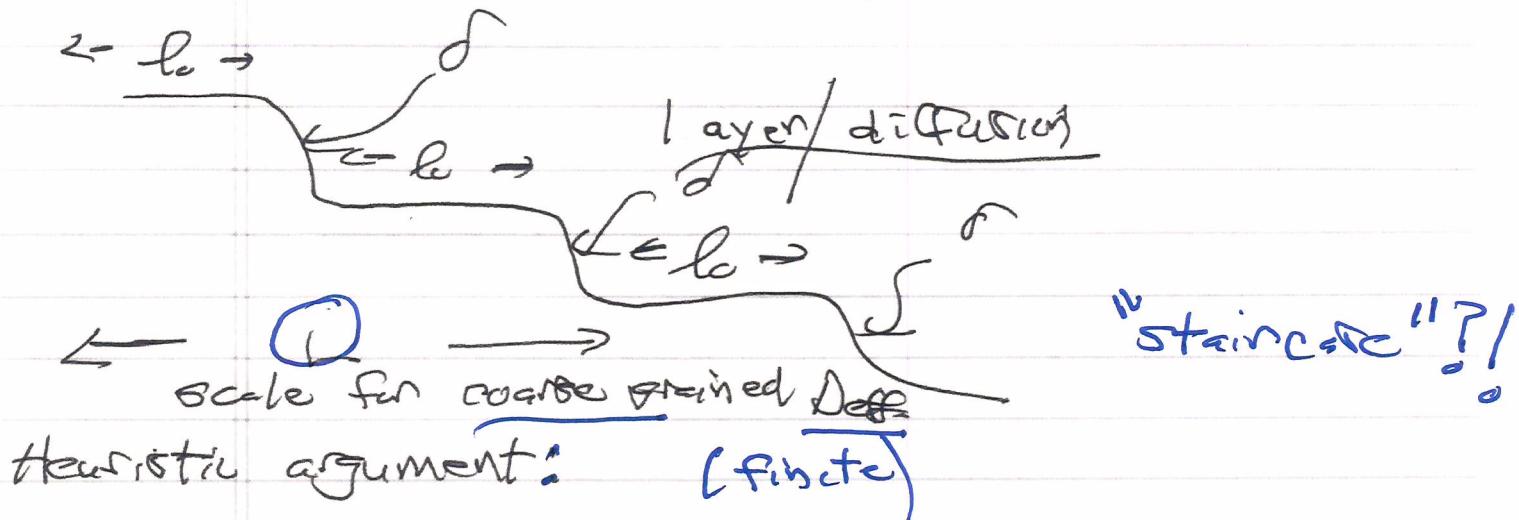
What is D_{eff} ?

Point: - transport is hybrid of

- diffusion is ultimate origin of irreversibility for static cells. Only BZ particles transported.
- fast kicks thru cell
- slow diffn thru BL

~~10~~

Can envision concentration profile:



→ for random walk:

↗ fraction of active region →

$$D_{eff} \approx \text{active } \frac{(\Delta x)^2}{\Delta t}$$

fraction where diffusion occurs.

Factor: active fraction for diffusion

$$\sim \underline{\delta/l_0}$$

small in δL thickness

Δt : cell circulation time

$$\sim \underline{l_0/V_0}$$

then

$$\delta^2 \sim D_0 \Delta t \sim D_0 \frac{l_0}{V_0}$$

Diffusing
in transit
time thru
layer

4.

and $\Delta X \sim l_0$ (cell scale).

so

$$D_{eff} \approx \frac{d}{l_0} \frac{l_0^2}{l_0/l_0}$$

$$\approx \left(\frac{D_0 l_0}{V_0} \right)^{1/2} \frac{l_0}{l_0} V_0$$

$$\approx (D_0 V_0 l_0)^{1/2}$$

$$= \boxed{D_0 (R_e)^{1/2}}$$

$$D_{eff} \approx (D_0 D_{cell})^{1/2}$$

→ D_{eff} is geometric mean of D_0 (star) and D_{cell} (flat), $\approx R_e^{1/2}$, large R_e

→ resembles Dykhne result, but
→ Dykhne → equal areas T_1, T_2
cells → $D_{active}/l_0 \ll 1$

→ see Rosenbluth et al. 1987 for details of calculation (tedious)

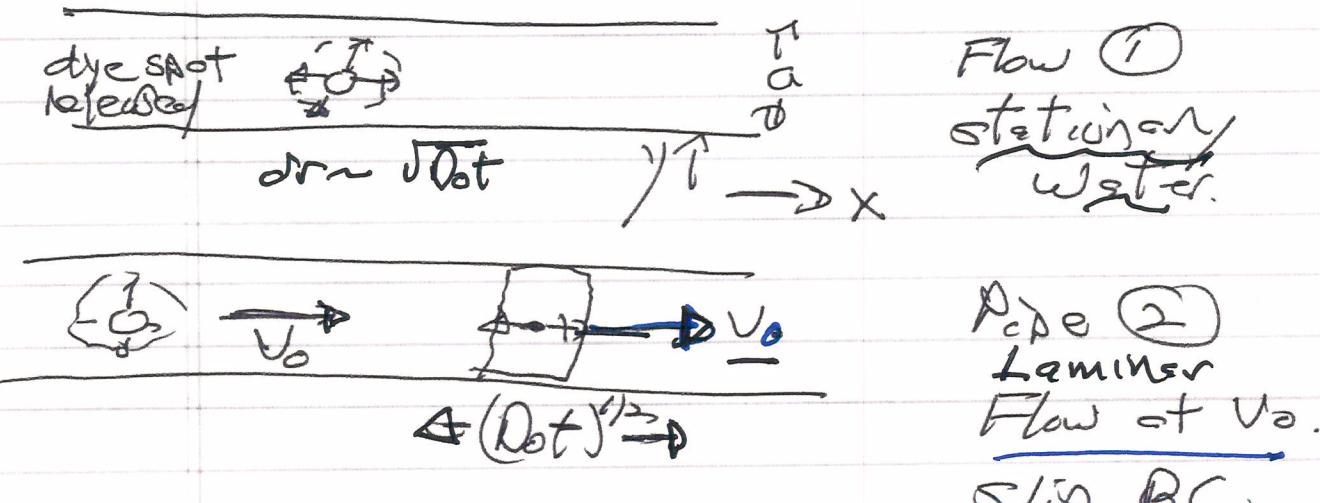
→ Result is not simple addition

5. F

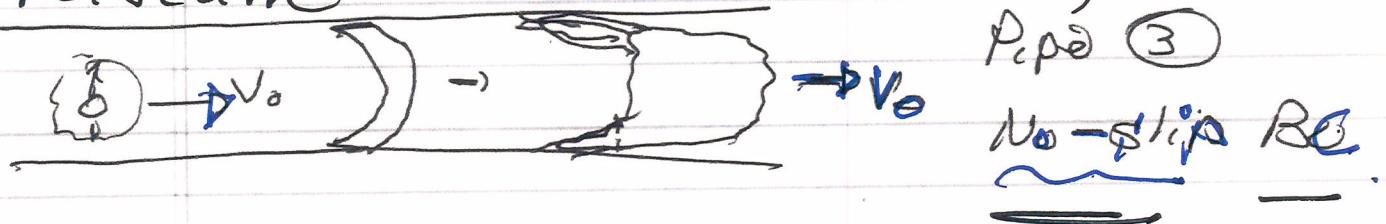
Related problem: Shear dispersion

see Taylor 1953 et seq. (many postings)
 Young & S. Jones especially good

Problem stated by comparison of three laminar flows, into which dye with molecular diffusion D_a is injected.



necessarily a shear flow.
Poiseuille - Laminar



Pipe ②: - plug CM advects at U_0

- plug expands axially at $(Dot)^{1/2}$ \Rightarrow molecular diffusion

δ_{as}

Shear Dispersion:

→ What is effective along stream
diffusivity of passive scalar
in a laminar shear flow.

Simpson - Poiseuille Flow

- BC \rightarrow shear

"the fundamental character of
the result that differentiates
unidirectional convection and
transverse diffusion yield a
longitudinal diffusion process
far downstream"

6. ~~X~~

Laminar Flow

→ fact ③:

- experiments (cf. 1953 paper) indicate more rapid dispersion of dye in sheared flow, i.e. effective axial diffusion enhanced

$$D_{\text{eff}} \text{ axial} > D_0$$

$$\Rightarrow D_{\text{eff}} = D_0 + D_{\text{shear}}$$

why? $\leftarrow \rightarrow \perp = v_g$

$$\frac{\partial C}{\partial t} + \underline{v} \cdot \nabla C = D_0 \nabla^2 C \rightarrow \partial_t(C) + \partial_x(vC) =$$

- though CM velocity same v_0 ? $D_0 \nabla^2 C$

- Velocity shear stretches cloud,



spreading it more rapidly. Effect is $\underline{\text{shear}} + D_0$

How calculate?

\perp collisional scattering terms

Consider dye concentration field $C(x, y, t)$

Calculation - Simple

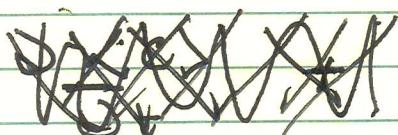
Now, consider scalar equation:

$$\frac{\partial C}{\partial t} + \underline{V} \cdot \underline{\nabla} C = D_0 \nabla^2 C$$

$$\langle C \rangle = \frac{1}{a} \int_{-a/2}^{a/2} dy C(x, y, t)$$

section
avg
(2D, 3D)

$$\langle V \rangle = \frac{1}{a} \int_{-a/2}^{a/2} dy V(y, t)$$



$$\frac{\partial C}{\partial t} + \underline{V} \cdot \underline{\nabla} C = D_0 \nabla^2 C \quad (1)$$

$$= D_0 (\partial_x^2 + \partial_y^2) C$$

$$\partial_t \langle C \rangle + \langle V \rangle \partial_x \langle C \rangle + \partial_x \langle \tilde{V} \tilde{C} \rangle \quad (2)$$

$$= D_0 \partial_x^2 \langle C \rangle$$

$$\tilde{V} = V - \langle V \rangle$$

$$\tilde{C} = C - \langle C \rangle$$

Now, subtract (2) from (1):

~~$\partial_t \langle C \rangle + \partial_x \tilde{C} + \langle v \rangle \partial_x \langle C \rangle$~~

$$\begin{aligned}
 & \partial_t \langle C \rangle + \partial_x \tilde{C} + \langle v \rangle \partial_x \langle C \rangle \quad (1') \\
 & + \tilde{v} \partial_x \langle C \rangle + \langle v \rangle \cdot \nabla \tilde{C} \\
 & + \partial_x \langle \tilde{v} \tilde{C} \rangle + D \cdot \nabla \tilde{C} \\
 & = D_0 (\partial_x^2 \langle C \rangle) + D_0 \partial_x^2 \tilde{C} \\
 & + D_0 \partial_y^2 \cancel{\langle C \rangle} + D_0 \partial_y^2 \tilde{C}
 \end{aligned}$$

$$\begin{aligned}
 & \partial_t \langle C \rangle + \langle v \rangle \partial_x \langle C \rangle + \partial_x \langle \tilde{v} \tilde{C} \rangle \quad (2') \\
 & = D_0 \partial_x^2 \langle C \rangle
 \end{aligned}$$

subtracting:

$$\begin{aligned}
 & \partial_t \tilde{C} + \langle v \rangle \cdot \nabla \tilde{C} - D_0 \partial_y^2 \tilde{C} \\
 & + \tilde{v} \partial_x \langle C \rangle = D_0 \partial_y^2 \tilde{C}
 \end{aligned}$$

Define:

$$\left(\frac{d}{dt} \tilde{C} \right) = \partial_t \tilde{C} + \langle v \rangle \cdot \nabla \tilde{C} - D_0 \partial_y^2 \tilde{C}$$

$$\left(\frac{d\tilde{C}}{dt} \right) + \tilde{V} \partial_x \langle C \rangle = D_o \partial_y^2 \tilde{C}$$

Now,



→ Pipe has finite \perp scale

→ this defines a characteristic finite scale — in frame co-moving with $\overset{\text{mean}}{f}$ — of

$$\tilde{T}_{\text{diff}} \sim L_1^2 / D_o . \quad \left[\begin{array}{l} L_1 \ll L_{11} \\ \rightarrow \text{time scale separation} \end{array} \right]$$

For $t \gg \tilde{T}_{\text{diff}} \approx L_1^2 / D_o$,
diffusively damped.

So, time asymptotically, i.e.

$$t \gg \tilde{T}_1 \text{ diff}$$

have dominant balance:

$$\tilde{V}_x \partial_x \langle C \rangle \approx D_o \partial_y^2 \tilde{C}$$

$$\text{Recall: } \tilde{V}_x = V - \langle V \rangle$$

Fourier Expnd:

$$\tilde{C} = \sum_{k_y} e^{i k_y} \tilde{C}_{k_y}$$

\tilde{v} simclr.

$$k_y \text{ min} \cong 2\pi/L_L$$

⇒

$$\tilde{v}_{x_{k_y}} \partial_x \langle C \rangle = -k_y^2 D_0 \tilde{C}_{k_y}$$

$$\tilde{C}_{k_y} = \frac{-1}{k_y^2 D_0} \tilde{v}_{x_{k_y}} \partial_x \langle C \rangle$$

so, what is sought:

$$\langle \tilde{v}_x \tilde{C} \rangle = \sum_{k_y} -\frac{\tilde{v}_{x_{k_y}}^2}{k_y^2 D_0} \underbrace{\partial_x \langle C \rangle}_{\partial X}$$

so, recalling:

$$\partial_t \langle C \rangle + \partial_x \langle \tilde{v}_x \tilde{C} \rangle = D_0 \partial_x^2 \langle C \rangle$$

so $D_{\text{eff}} = D_0 + D_{\text{shear}}$

$$D_{\text{shear}} = \sum_{k_{ij}} \tilde{W}_{ij} l^2 / k_{ij}^2 D_0$$

$$\Rightarrow \# \frac{V_0^2 L_1^2}{D_0}$$

$$D_{\text{eff}} = D_0 + D_{\text{shear}}$$

$$= D_0 + \# \frac{V_0^2 L_1^2}{D_0}$$

Note that for Laminar flow

$D_{\text{shear}} > D_0$ quite possible

\Rightarrow enhanced along stream / in frame diffusivity.

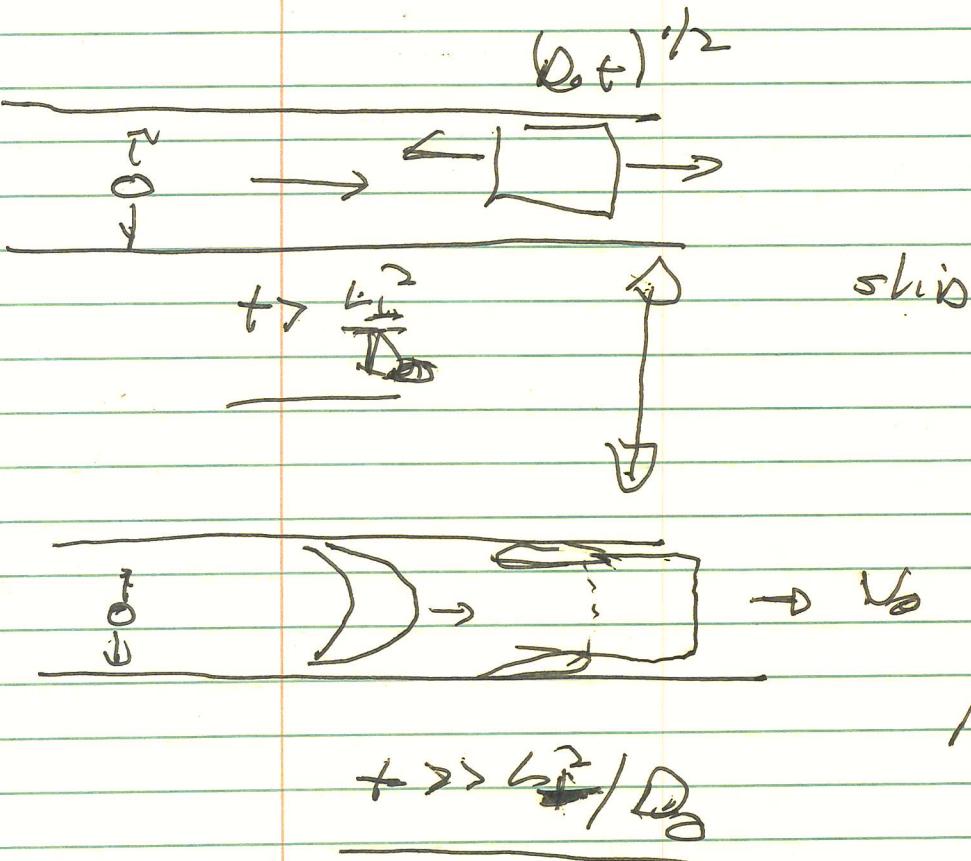
\Rightarrow enhanced dispersion / shear dispersion ^u

Seven Points:

→ What is happening?

"the fundamental character of the result [differential unidirectional convection and transverse diffusion] yield a longitudinal diffusion process far downstream"

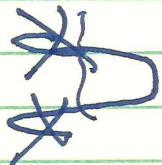
i.e.



→ asymptotic result:

$$+ \gg L_1^2 / D_0$$

→ uni-directional velocity essential



→ Details:

$$v(y, z) = 2(u/a^2)(a^2 - y^2 - z^2)$$

$$\# = 1/48$$

$$D_{eff} = D_o + \frac{1}{48} \frac{V_o^2 a^2}{D_o}$$

$$D_{sh} > D_{eff} \text{ for } P_o > \sqrt{48} \quad \checkmark$$

→ For turbulent flow,

$$\Delta_{shear} \sim \# \frac{U_f^2 a^2}{D_{shear}}$$

$$D \sim U_f a$$

More generally:

- Origin of irreversibility is D_o
(laminar flow) . $T_c^{-1} \sim D_o / t_{\lambda}^2$
- A living cell, laminar flow +
molecular diffusion yields transport.
- Taylor proposed shear dispersion
as mechanism for distributing
nutrients in blood flow.
- time scale ordering is crucial.
- Excellent topic for further
study.

To Percolation \rightarrow

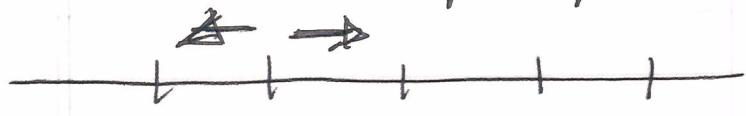
15.



Percolation processor I

Percolation vs. Diffusion \rightarrow Comparison / Contrast

a.) Diffusion \Rightarrow 1D random walk
prob. $1/2$ for each way, each step



- medium fixed

- particle motion stochastic

$$\langle \Delta x^2 \rangle \sim D t$$

$$\sim N$$

\hookrightarrow # steps

and particle returns.

b.) Percolation - assign left/right orientation to each site; with probability $1/2$

particle



- medium stochastic

- particle motion deterministic

i.e. random conductivity

Ko

Simpler: \rightarrow diffusion; medium deterministic,
motion stochastic $k_u < 1$

\rightarrow percolation; motion deterministic,
medium stochastic $k_u > 1$

Examples:

\sim "random" media
at low, high k_u .

a.) Cascade process

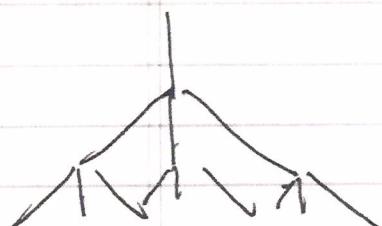
$$(p + \bar{z}) = 1$$



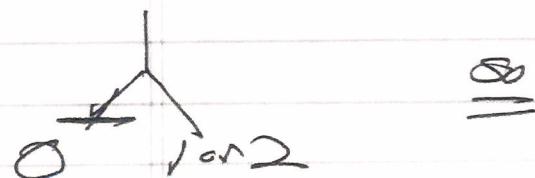
descendant

$$\text{Order: } 1 \text{der}, 2 \text{der} \\ \Rightarrow 2PZ \quad P^2$$

can think of as diffusion

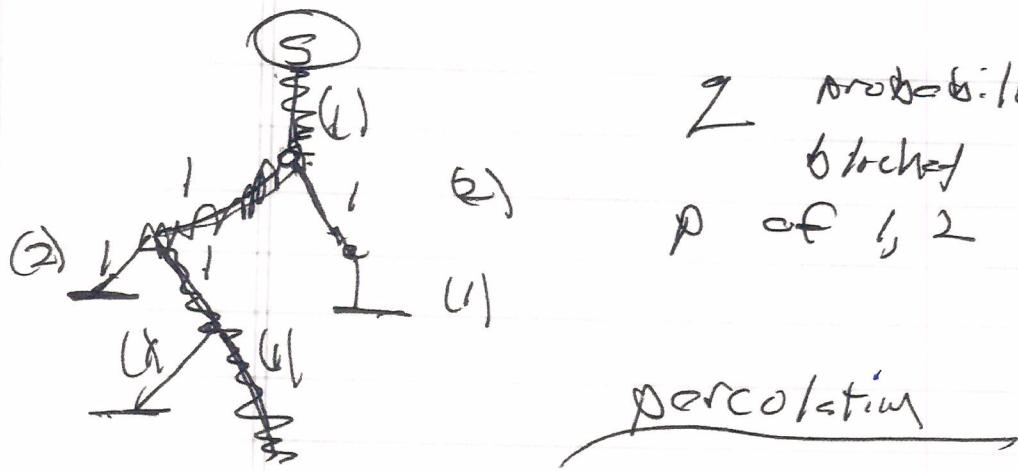


at, does one generation "reach" N into
future



\otimes

$=$

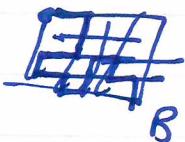


In Percolating:

- intensive and random properties of medium determine motion. (i.e. cell arrangement)
- is diffn / stoch motion indeterminate. Prop. particles fundamental (i.e. stochastic orbits).

Origin of random characteristics of medium:

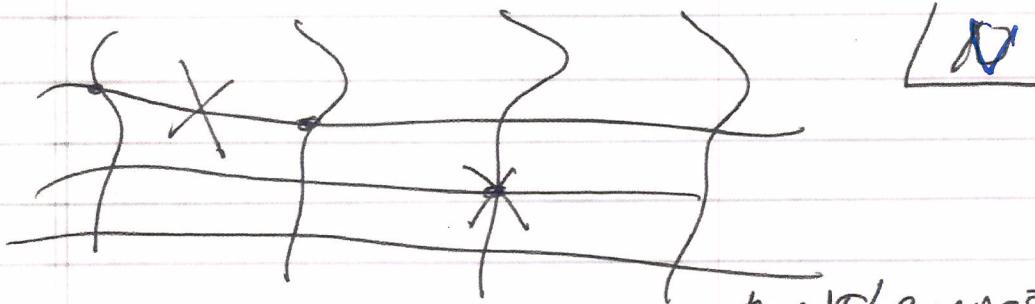
- randomly dam / cut connections
Dimensionality matters
- result is random maze
- flow can traverse $A \rightarrow B$ only if there is an un-dammed un-cut self-avoiding random walk connecting A, B
SAW visits intermediate at most once.



→ General aspects (mostly topological)

- can have bond "or site" percolation

C.e



bonds/connections

bond \rightarrow some fraction of ~~sites~~ missing

site \rightarrow some fraction of sites missing

\Rightarrow game played either way.]

- Consider:

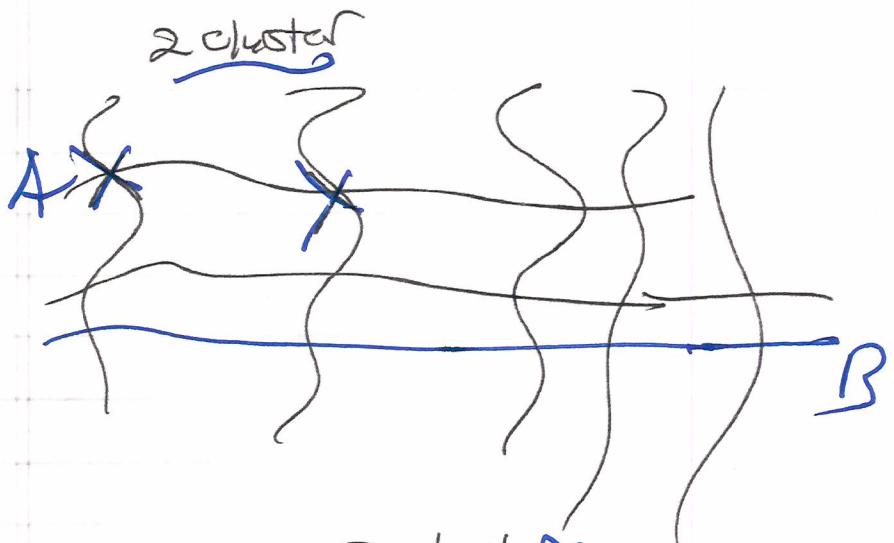
\rightarrow lattice of N sites, $N \gg 1$

\rightarrow concentration of allowed
sites X

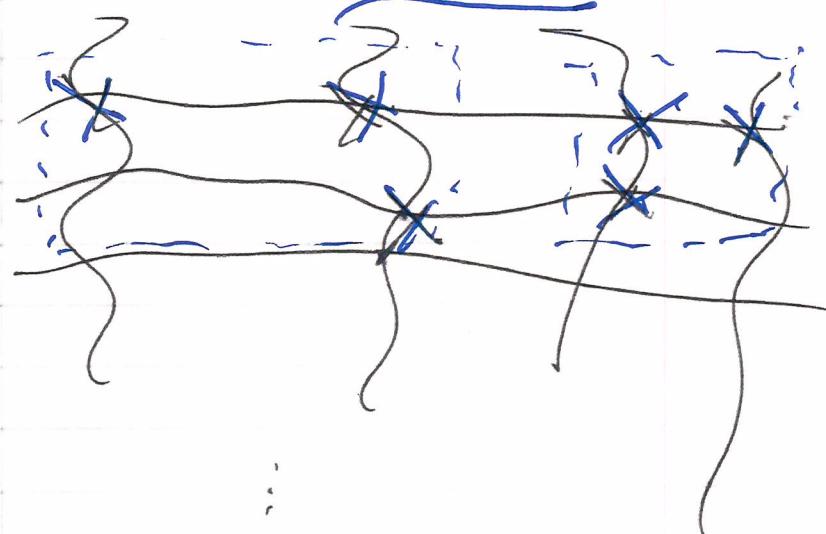
\Rightarrow can envision increasing X
from below, i.e.

19

i.e.

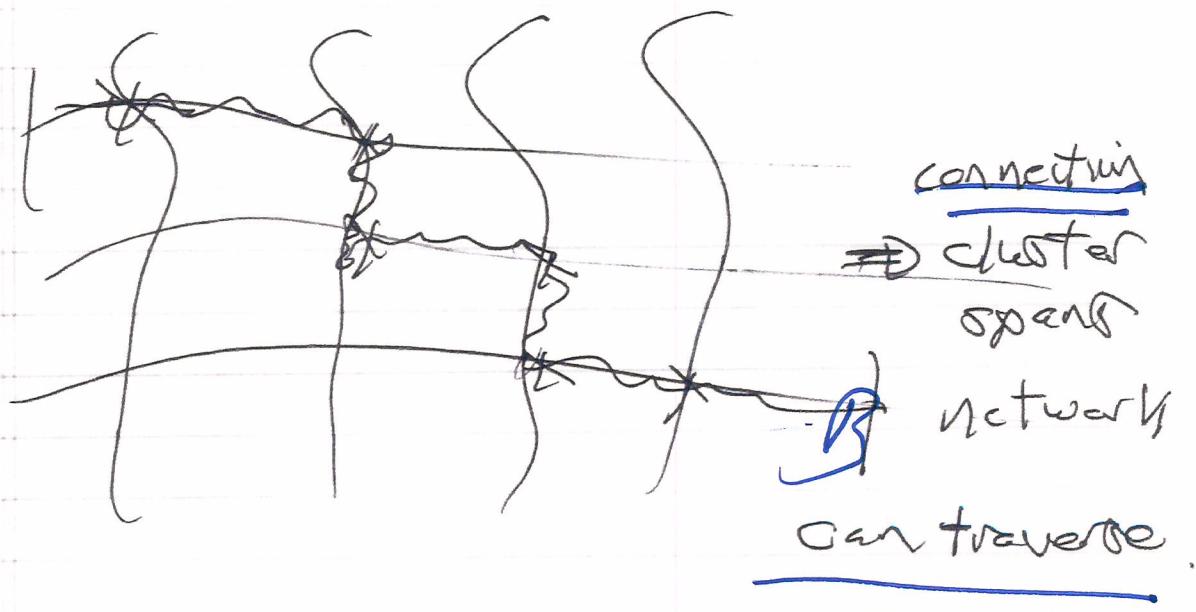


3 clusters



$N \gg 1$

:



Q2 $N \rightarrow \infty$.

- $x < x_c \rightarrow$ isolated small clusters
- $x \uparrow \rightarrow$ larger clusters form.
- $\ell(x) \uparrow$ with x
 \uparrow
 size
- as $x \uparrow$, few large clusters form
- $\ell(x_c) \rightarrow \infty$ as $N \rightarrow \infty$
- one cluster for $x > x_c$

Phase transition

$P^S(x) \equiv$ site percolation probability

\equiv [ratio of # sites in big (infinite)
cluster to # sites in lattice]

\equiv [fraction of system in which
AC conduction is possible.]

And:

- there is a threshold concentration of active sites, x_c
- near threshold:

$$P^s(x) \sim (x - x_c)^{\beta}$$

percolation exponent

geometric universality

[
fraction conducting]
- 3D: $\beta \sim .3 \rightarrow .4$
 [intermediate lattice structure]
- ⇒
 - percolation is a type of phase transition
 - α_c , $\delta \rightarrow$ critical exponent
 - $x_c \rightarrow$ critical temp / pt.
 - $\beta_A \sim \beta_c$.
- key question is effective medium model near x_c .
- connection to turbulence: intermittency → reduced packing fraction.