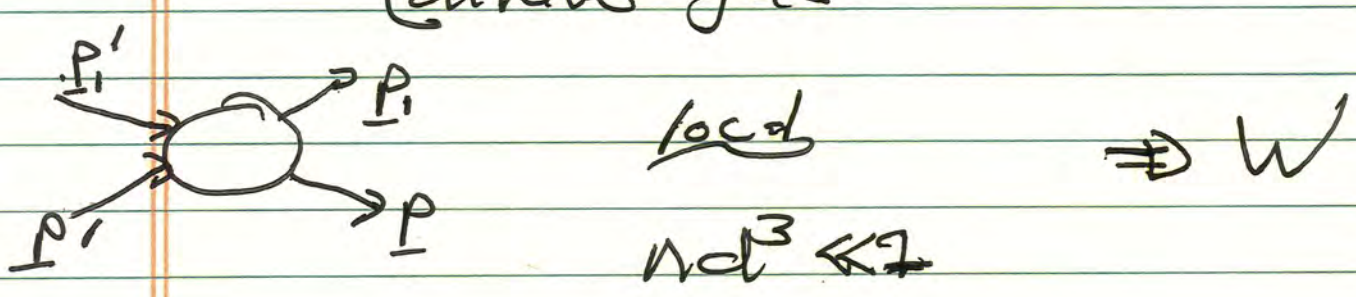


Notes I ; Section III

- Fluid Equations (Ideal)
- Transport Coefficients
- Viscous Fluids

Recall:

- classical, { hard sphere interaction
 dilute gas



- Boltzmann Equation

$$\frac{\partial f}{\partial t} + \underline{v} \cdot \nabla f = C(f)$$

$$C(f) = \int d\underline{p}' \int d\underline{p}_i' \int d\underline{p}_i \left[f(\underline{p}) f(\underline{p}_i') - f(\underline{p}_i) f(\underline{p}) \right] W(\underline{p}_i', \underline{p}_i'; \underline{p}, \underline{p}_i)$$

- use: { $n d^3 r \ll 1$
 detailed balance
 Molecular chaos

↓
 transition probability

- cont'd to truncate BBGKY hierarchy.

⇒ Eqn. $F(x, t)$.

H - Theorem

$S = \int dx S = \int dx dp (-F \ln F)$
- entropy

showed:

$\frac{dS}{dt} \geq 0$

Macroscopic order from microscopic reversibility and molecular chaos.

key: Detailed Balance
Molecular Chaos

Some up-shots:

- $\frac{dS}{dt} = 0 \Rightarrow \frac{dS}{dt} = 0$

locally $f' f_1' = f_1 f$

⇒ $\ln f' + \ln f_1' = \ln f_1 + \ln f$

so at equilibrium, $\ln f$ must be additive for collision,

Q collision operator conserves:

- number
 - momentum
 - energy
- and must be normalizable.

$$\ln f = c + \alpha \underline{V} \cdot \underline{p} - \beta E$$

$$E_1 + E_2 = E_1' + E_2'$$

$$\underline{p}_1 + \underline{p}_2 = \underline{p}_1' + \underline{p}_2'$$

$$\beta > 0$$

$$f_0 = c n_0 \exp \left[- \frac{(E - \underline{p} \cdot \underline{V})}{T} \right]$$

equilibrium is Maxwellian.

- i.e. local equilibrium, scale $\ln f$

$$f = c n_0(x) \exp \left[- \frac{(\underline{v} - \underline{v}(x))^2 m}{T(x)} \right]$$

$n \rightarrow$ density

$\underline{V} \rightarrow$ flow

$T \rightarrow$ temperature

Note:

f_{eq} local
does not

solve Boltzmann
equation unless

$$\underline{V} \cdot \nabla f_{eq} = 0$$

(homogeneous)

- "global equilibrium"

n, T, \underline{V} constant.

$e(f)$ \rightarrow drives to local
equilibrium on
collision time scale

Inhomogeneity

\rightarrow
deviation from
maximum
entropy state.

$$\tau_C \sim \frac{v_{th}}{l_{mp}} \sim \frac{v_{th}}{v_{th} n \lambda} \sim \frac{1}{n \lambda}$$

$$\text{Result } W \sim v_{rel} dT.$$

\rightarrow global equilibrium on

$$\frac{1}{\tau_{relax}} \sim \frac{D}{L^2} \sim \frac{v_{th} l_{mp}}{L^2}$$

$$\frac{1}{T_{\text{relax}}} \sim \sqrt{L} \left(\frac{l_{\text{MFP}}}{L} \right)^2 \quad T_0 \ll T_{\text{relax}}$$

Result: $d \ll \bar{r} \ll l_{\text{MFP}} \ll L$

Global Relaxation \Rightarrow transport!
 \rightarrow how calculate transport coefficients?

N.B. - Collision is local (Stohm - enstz) - $d \ll l_{\text{MFP}}$ -
 so establish local equilibrium
 on τ_0^{-1} scale

- Later relax to constant n, T, \underline{v}

Simplified Collision Operator

\rightarrow Collision operator is nonlinear and complex.

→ convenient to use reduced form:

$$\frac{\partial F}{\partial t} + \underline{v} \cdot \nabla F = C(F)$$

$$= -\nu_{\text{eff}} (F - f_{\text{eq}})$$

$f_{\text{eq}} \rightarrow$ local Maxwellian. ($f_{\text{eq}} \neq f$)

$\nu_{\text{eff}} = \nu =$ collision frequency

⇒

$C(F)$ as local relaxation process

- Krook Model, Operator

BGK Model: $\left\{ \begin{array}{l} \text{Bhatnagar} \\ \text{Gross} \\ \text{Krook} \end{array} \right.$

(\neq BGK model, please)

- also a "Crook" model

- does not conserve momentum, energy

- nonlinearity buried.

⇒ Kinetic models are crooked, but useful.

⇒ How use Boltzmann Eqn?

- f evolution → GD (Aeinfeld).

- recall scale ordering:

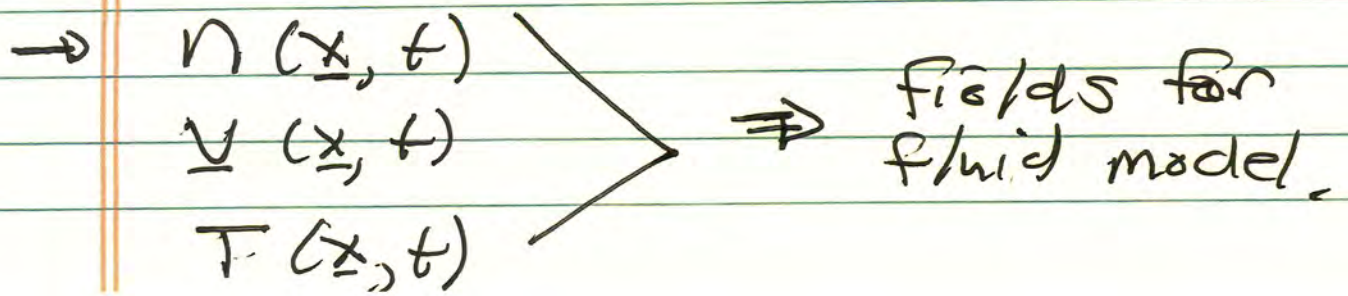
$$d \ll \bar{r} \ll l_{mfp} \ll v_{th}$$

100

For $\lambda \geq l_{mfp}$ — macroscopic scales

Why solve for f ? — $f \sim f_{eq}$.

Solve for parameters of f_{eq}



$$k_b = 1.$$

8. 

→ Fluid Equations

not a substitute
for proper
study of fluid
mechanics

- what to do with B.E. ⇒

{ fluid eqns. ΔB
transport coefficients → flux-force proportionality
 $\vec{T} = -\eta \nabla \vec{v}$

- replace B.E. by set of equations which
evolve thermodynamic parameters. (for param.)

⇒ hydrodynamic equations for $n(\vec{x}, t)$, $\vec{v}(\vec{x}, t)$,
 $P(\vec{x}, t)$ etc.

- local, Eulerian description (lab frame)
held together by collisions, vs. dispersion

- describes 'blobs' of gas, held together by
collisions, $L > \text{lmfp}$

fluid element $\omega < r_{\text{coll}} >$ scales of
relevance

- parameterized dynamics in terms
structure of distribution

$$f \equiv \frac{n(\vec{x})}{(2\pi T)^{3/2} v_{\text{th}}(\vec{x})^3} \exp \left[-\frac{(\vec{v} - \vec{v}(\vec{x}, t))^2}{v_{\text{th}}^2(\vec{x}, t)} \right]$$

$n, \vec{v}, T; P = nT$

- works for slight deviation from
equilibrium.

Total Distr:

i.e. $f = f_{eq} + \delta f$

↓
local
Maxwellian
↓
ideal
equations

↳ $\delta f = -\frac{\mathbf{v} \cdot \nabla f}{v} \sim \text{linear } \nabla f$

↓
viscous
dissipative
eqns.

sacrifices info re: higher moments (usual energy truncation). → why core? i.e. heat flux, beyond?

now, recall:

$$\frac{\partial f}{\partial t} + \mathbf{v} \cdot \nabla f = \epsilon(f)$$

demand: $\int d^3v C(f) = 0$ (# conservation)

(easily shown) $\int d^3v m \mathbf{v} C(f) = 0$ (momentum conservation)

$\int d^3v \epsilon C(f) = 0$ (energy conservation)

then define:

$n = \int d^3v f \rightarrow$ density

$\mathbf{v} = \frac{1}{n} \int d^3v \mathbf{v} f \rightarrow$ velocity / momentum



$$\bar{E} = \frac{1}{n} \int d^3V \epsilon f \rightarrow \text{energy density}$$

phase space
↓

$$\text{and } \partial_t f + \partial_{x_i} (v_i f) = c(f)$$

taking moments:

conservative form

$$\frac{\partial n}{\partial t} + \nabla \cdot (n \underline{v}) = 0$$

mass flux # cons.

(number conservation)

$$\frac{\partial}{\partial t} (m v_\alpha) + \frac{\partial}{\partial x_\beta} \Pi_{\alpha\beta} = 0$$

↓ ↓
MOM. cons.

(momentum balance)

[momentum flux]

$$\Pi_{\alpha\beta} = \int d^3V m v_\alpha v_\beta f$$

$$\frac{\partial (n \bar{E})}{\partial t} + \nabla \cdot \underline{z} = 0$$

energy flux energy cons.

(energy balance)

$$\underline{z} = \int d^3V v \epsilon f$$

note form:

conservation

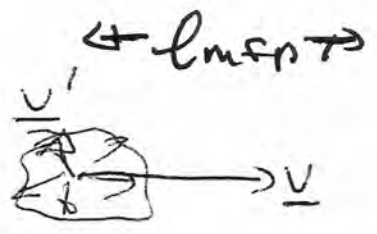
$$\frac{\partial}{\partial t} (\text{stuff}) + \nabla \cdot (\text{Flux of stuff}) = 0$$

→ essence is calculation of fluxes,

Further simplify by:

$$\underline{v} = \underline{V}(\underline{x}, t) + \underline{v}'$$

mean/bulk flow
(~ linked to body forces)
thermal fluctuation
about mean
(~ $\sqrt{T/m}$)



realistically:
 $|\underline{v}| \ll |\underline{v}'|$

{ but \underline{v}' 's cancel }

so

$$\Pi_{\alpha\beta} = \int d^3V m (v_\alpha(\underline{x}, t) + v'_\alpha) (v_\beta(\underline{x}, t) + v'_\beta) f$$

$f = f_{cl} + f'$ ↗ here ↔ "ideal" fluid.

loc. Maxwellian, as above. → neglected

so

$$\Pi_{\alpha\beta} = mn (v_\alpha(\underline{x}, t) v_\beta(\underline{x}, t) + \langle v'_\alpha v'_\beta \rangle)$$



now, $f = \frac{n(x)}{(2\pi)^{3/2} v_{th}^3(x)} \exp \left[-\frac{(v - \underline{v}(x,t))^2}{v_{th}^2(x)} \right]$

(assumption?)

$\langle v'_\alpha v'_\beta \rangle = \frac{1}{3} v^2 \delta_{\alpha,\beta}$ (isotropic eq $\frac{dv}{dt}$)

$\langle v'^2 \rangle = 3T/m$

(collisions isotropize pressure)

so, can define:

$\underline{p} = mn \langle v'_\alpha v'_\beta \rangle$

~~stress~~ stress tensor

$= \frac{1}{3} mn \langle v^2 \rangle \delta_{\alpha,\beta}$

$p = nT$

(Diagonal for ideal fluid)

so

$\frac{\partial}{\partial t} (n\underline{v}) + \underline{\nabla} \cdot (n\underline{v}\underline{v} + \underline{I} p) = 0$

but: $\frac{\partial n}{\partial t} + \underline{\nabla} \cdot (n\underline{v}) = 0$

Euler Eqn:

subtracting \Rightarrow

$n \left(\frac{\partial \underline{v}}{\partial t} + \underline{v} \cdot \underline{\nabla} \underline{v} \right) = -\underline{\nabla} p$

"Euler Eqn."

(+ visc \rightarrow Navier-Stokes)

incompressible $\underline{\nabla} \cdot \underline{v} = 0$

$\underline{\nabla} \cdot \underline{v} = 0$ defines ρ (incompressible fluid).

Similarly,

$$E = \frac{1}{2} m v^2 + e'$$

$$= \frac{1}{2} m (\underline{v}(x,t) + \underline{v}')^2 + e'$$

$$\begin{aligned} \underline{Z} &= \int e v f d^3 v \\ &\equiv \int e v f_0 d^3 v \end{aligned}$$

$$\begin{aligned} \underline{Z} &= \int d^3 v (\underline{v}(x,t) + \underline{v}') (e' + \frac{1}{2} m (\underline{v}(x,t) + \underline{v}')^2) f \\ &= \underline{v}(x,t) \left(\frac{1}{2} m n \bar{v}^2 + \underbrace{p + n e'} \right) \end{aligned}$$

\hookrightarrow $w +$ ~~enthalpy~~ enthalpy

3

$$\frac{\partial}{\partial t} (n \bar{E}) + \underline{\nabla} \cdot \left[\underline{v}(x,t) \left(\frac{1}{2} m n \bar{v}^2 + p + n e' \right) \right] = 0$$

\downarrow
can simplify
as for momentum.

→ angular momentum not conserved by $c(f)$



→ most truncations stop at 3rd moment

Now, for transport: Flux - Gradient Relations!

→ what if f_0 has gradient? $T(x)$
 ⇒ driven off

i.e. Chapman-Enskog expansion
 ⇒ $df = -\frac{1}{v_c} \nabla \cdot \nabla f_{eq}$

→ then $f_0 + df$ set fluxes, so

Flux = f_{eq} (ideal part) + df (collisional part) ⇒ transport.

Key Point: How relate fluxes to gradients in thermodynamic quantities?

Non-Ideal Fluids, Transport, Chapman-Enskog (Viscous)

Applications of the Boltzmann Equation

→ Chapman-Enskog → Basis (C-E Light)

- a major application of B.E. is calculation of transport coeffs.

- recall, fluid equations involve momentum, heat flux

i.e. really $\frac{\partial U}{\partial t} = -\nabla \cdot \underline{\underline{\Pi}}$, etc.

continuity form

here:

$$\Pi_{\alpha\beta} = mn (u_\alpha u_\beta + \langle u'_\alpha u'_\beta \rangle)$$

$$\langle u'_\alpha u'_\beta \rangle = \int d^3v f u'_\alpha u'_\beta$$

if $f = f_{02} = \frac{n(x)}{(2\pi)^{3/2} v_{th}(x)^3} \exp\left[-\frac{(v-v(x))^2}{2v_{th}^2}\right]$

⇒ $\langle u'_\alpha u'_\beta \rangle = \frac{1}{3} \langle v^2 \rangle \delta_{\alpha\beta}$

$$\langle v^2 \rangle = 3T/m$$

but is $f = f_{02}$? ?

Recall, f satisfies:

$$\partial_t f + \underline{v} \cdot \underline{\nabla} f = C(f)$$

f_{eq} is soln. to $C(f) = 0$.

\Rightarrow f_{eq} cannot solve B.E. unless $\underline{\nabla} f_{eq} = 0$!

can assign time scales:

$$\partial_t f \rightarrow \omega$$

$$\underline{v} \cdot \underline{\nabla} f \rightarrow v_{th} / L$$

$$C(f) \rightarrow \nu$$

Collisional regime has $\nu > \frac{v_{th}}{L}$
 $d < \bar{r} < l_{mfp} < L$

$$\nu = \frac{v_{th}}{l_{mfp}} \quad \frac{v_{th}}{L} < \nu$$

$$l_{mfp} = 1 / n \nu$$

\Rightarrow f_{eq} is 0th order solution.

then if f_0 is homogeneous \Rightarrow

stationary solution has correction!

$$f = f_0 + \delta f$$

\hookrightarrow ~ inhomogeneity
 i.e. $\nabla T, \nabla V$

more precisely response to inhomogeneity

$$\text{and } \langle \underline{v} \underline{v}' \rangle = \int d^3V (f_0 + \delta f) \underline{v} \underline{v}'$$

$$= \rho \underline{\alpha}_{\alpha\beta} + \underline{\text{Viscous stress}}$$

$$\sim \nabla V$$

viscosity $\sim \mu D$

d.e. $\mu n \langle v_x' v_x' \rangle_{visc} = -\eta \frac{\partial \langle v_x \rangle}{\partial x}$

$= -\eta \frac{\partial \langle v_x \rangle}{\partial x} + \dots$
 $D \sim \text{length}$

so, need:

↳ generic form of viscous stress

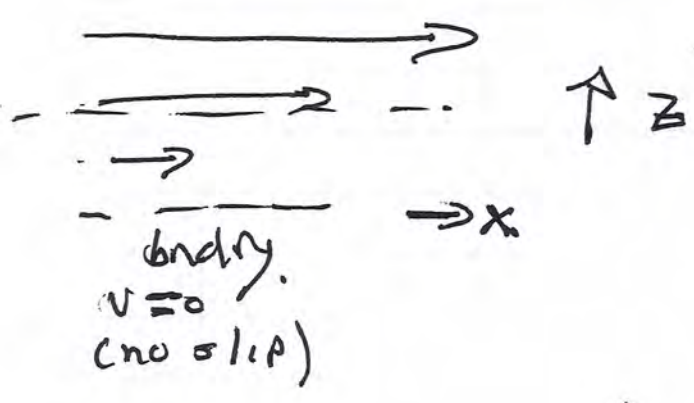
Flux-Gradient

- understand viscosity, etc.
- see how calculate η and then transport coeffs (viscosity)

so what is viscosity about?

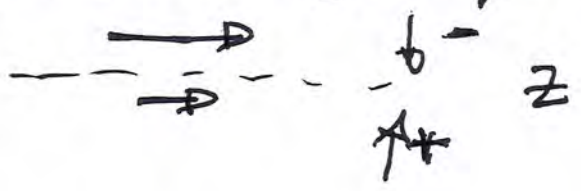
= simple physics of transport coeffs!

consider collisional gas:



mean flow
 \downarrow
 $\underline{v} = v(z) \hat{x}$
 i.e. shear flow
 (gradient \perp flow)

choose imaginary surface:





Calculate transport of \vec{x} momentum thru surface:

$$\pi_+ = \int_{v_z > 0} d\underline{v} m v_x v_z f$$

$$\sim v_{\text{th}} \bar{v} n m v_+$$

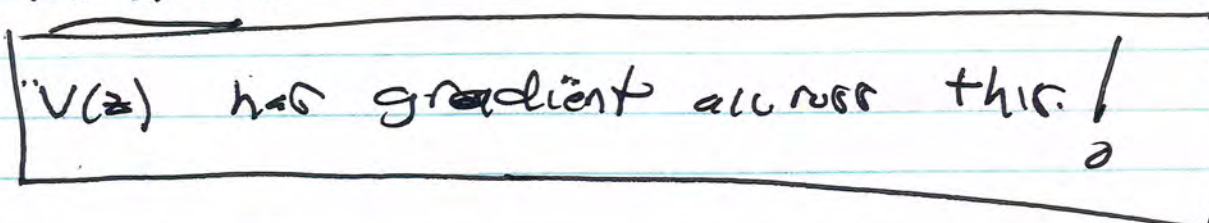
$$\pi_- = \int_{v_z < 0} d\underline{v} m v_x v_z f$$

at first glance, would expect $\pi_+ = \pi_-$

so $\pi_{\text{tot}} = 0$! but :

--- \Rightarrow  E_{ex}

\rightarrow "scale of resolution" for imaginary surface is $\text{Impp} \Rightarrow$ defines effective thickness.

\rightarrow  $V(z)$ has gradient across this!

$$\stackrel{\infty}{=} \pi_{\text{tot}} = \pi_- + \pi_+$$

18

π_-

$$\pi \approx -nm v_{th} \bar{V}(z + \frac{l_{mp}}{2}) + nm v_{th} \bar{V}(z - \frac{l_{mp}}{2})$$

π_+

$$\approx -nm v_{th} l_{mp} \frac{\partial \bar{V}}{\partial z}$$

$\rightarrow \sim l_{mp} v_{th}$

$$\approx -nm D \frac{\partial \bar{V}}{\partial z}$$

$$= -\eta \frac{\partial \bar{V}}{\partial z}$$

viscosity (shear)

$$\sim \rho D$$

$$D \sim v_{th} \tau$$

→ Key Points:

- equal # collisions, kicked in +, - directions, but

- more momentum kicked down from above, due velocity gradient.

⇒

- net viscous momentum transport via collisions, to relax gradient



How calculate systematically?

⇒ Chapman - Enskog expansion!

now

$$\frac{\partial f}{\partial t} + \underbrace{\mathbf{v} \cdot \nabla}_{\frac{v_{Th}}{L}} f = C(f) \quad \left\{ \begin{array}{l} \text{multiple} \\ \text{time} \\ \text{scales} \end{array} \right.$$

$v > \frac{v_{Th}}{L}$

f normalization

and seek:

$$\Pi_{z,x} = \int d^3v \mathbf{v}_z (m v_x f)$$

\mathbf{z} direction flux of \mathbf{x} momentum

$$f = f_0 + df$$

$$\Pi_{z,x} = \int d^3v \mathbf{v}_z (m v_x (f_0 + df))$$

$$\text{if } f_0 \approx \frac{n_0}{v_{Th}^3} \exp \left[- \frac{(\mathbf{v} - v(z)\hat{x})^2}{2 v_{Th}^2} \right]$$

(i.e. local Maxwellian)

→ $f_{\theta z}$ contribution vanishes by symmetry!

so

$$\Pi_{z,x} = \int d^3x \cdot v_z (m \cdot \cancel{v_x}) \cdot dF$$

↑
drives the flux.

How get dF ?

⇒ Perturbative solution!

$$\nabla \cdot \nabla f = C(f) \rightarrow \left\{ \begin{array}{l} \text{really an} \\ \text{integral} \\ \text{equation!} \end{array} \right.$$

b. o. : $C(f) = 0$

$$f = f_{\theta z} \rightarrow \underline{\text{Local Maxwellian}}$$

1st o. :

$$\nabla \cdot \nabla f_0 = C(f_0)$$

$$\therefore dF = C^{-1} [\nabla \cdot \nabla f_0]$$

How?

→ lengthy calculation ~~XXXXXXXXXX~~

→ Krook (Crock) Model ↓

$$C(f) = -\nu (f - f_{eq})$$

↓
collisional decay to
(local) Maxwellian
Convect Empty ↓

or

$$\underline{v} \cdot \underline{\nabla} f = C(f) = -\nu (f - f_{eq})$$

$$f = f_{eq} + df$$

$$\underline{v} \cdot \underline{\nabla} (f_{eq} + df) = -\nu (f - f_{eq})$$

$$\text{l.o.} : -\nu (f - f_{eq}) = 0$$

$$f = f_{eq}$$

1st order :

$$\underline{v} \cdot \underline{\nabla} f_{eq} = -\nu df$$

$$df = - \frac{\underline{v} \cdot \underline{\nabla} f_{eq}}{\nu}$$

↓
perturbative
correction to f_0 ; $O\left(\frac{v_{th}}{L\nu}\right)$

18

$$\Pi_{z,x} = \int d^3v v_z m v_x dF$$

$$= \int d^3v v_z n m v_x \left(-\frac{v_z}{r} \frac{\partial}{\partial z} f_0 \right)$$

$$\vec{V} \vec{x} = V(z) \vec{x}$$

now $f_0 \approx \frac{n(x)}{V_{th}^3(x)} \exp \left[-\frac{(v - V(z) \vec{x})^2}{2 V_{th}^2(x)} \right]$

$$= \frac{n}{V_{th}^3} \exp \left[-\frac{(v - V(z))^2}{2 V_{th}^2} \right]$$

$$\frac{\partial f_0}{\partial z} = \frac{n}{V_{th}^3} \frac{v_x}{V_{th}^2} \frac{\partial V(z)}{\partial z} \exp [\quad]$$

linear response.

$$- 2 \frac{V(z)}{V_{th}^2} \frac{\partial V(z)}{\partial z} \exp [\quad]$$

dropped \Rightarrow
interested in only
linear response
of flux to
gradient.

see next

~~use the linear response to the flux to the gradient~~
~~is the only thing that matters~~
~~the rest is just noise~~

$$\frac{\partial f_0}{\partial z} = f_0 \frac{v_x}{V_{th}^2} \frac{\partial V(z)}{\partial z}$$

Note:

→ here seek linear relation between flux and gradient

→ assumes weak distortion from Maxwellian, i.e.

$$f_{eV} = \frac{n}{\sqrt{\pi}} \exp \left[-\frac{(v - v_D)^2}{2v_{th}^2} \right]$$

$$= \frac{n}{\sqrt{\pi}} \exp \left[-\frac{(v^2 - 2v v_D + v_D^2)}{2v_{th}^2} \right]$$

$$\approx \frac{n}{\sqrt{\pi}} \exp \left[-\frac{v^2}{2v_{th}^2} \right] \left[1 + \frac{v v_D}{v_{th}^2} \right]$$

$$= f_{e0} \left(1 + \frac{v v_D}{v_{th}^2} \right)$$

↑
e.o. Factor on expansion

yields result.

4 ϕ -coming → "Linear Response Theory"
Green-Kubo Relation

$$\Pi_{zx} = \int d^3x \, n_2 m v_x \left(-\frac{v_z}{r} \frac{v_x}{v_{Th}^2} \right)$$

$$\leftarrow \text{for } \frac{\partial V(z)}{\partial z}$$

$$= -\# \frac{m n}{r} v_{Th}^2 \frac{\partial V(z)}{\partial z}$$

$$= -\# m n \left(\frac{v_{Th}}{r} \right) v_{Th} \frac{\partial V(z)}{\partial z}$$

↳
lmp

$$D = v_{Th} \text{ lmp}$$

$$\Pi_{zx} = -\# m n D \frac{\partial V(z)}{\partial z}$$

$$= -\# \rho D \frac{\partial V(z)}{\partial z}$$

$$\eta = -\# \rho D$$

⇒ basic result for collisional shear viscosity

Note form of result:

$$\begin{array}{ccc}
 \Pi_{zx} & = & - \underbrace{\# n m D}_{\text{microscopic}} \frac{\partial V_x(z)}{\partial z} \\
 \downarrow & & \downarrow \\
 \text{Flux} & & \text{transport coefficient} \\
 & & \downarrow \\
 & & \text{thermodynamic force}
 \end{array}
 \quad \begin{array}{l}
 \leftarrow \text{gradient of} \\
 \text{thermo. quantity} \\
 \text{(dist.)} \\
 \downarrow \\
 \text{thermodynamic force.}
 \end{array}$$

⇒ example of thermodynamic flux-force relation.

⇒ constitutive relation is transport coefficient. proportionality

In general, have vector relation:

$$\begin{array}{ccc}
 \underline{\Gamma} & = & - \underline{A} \cdot \underline{\nabla} C \\
 \downarrow & & \downarrow \\
 \text{vector of fluxes} & & \text{vector of gradients} \\
 & & \downarrow \\
 & & \text{matrix of transport coefficients - Onsager matrix} \\
 & & (\text{n.b. Onsager symmetry} \rightarrow \underline{A} \text{ symmetric})
 \end{array}$$

⇒ Observe:

- F_{Max} annihilates collision operator,

and corresponds to $\frac{dS}{dt} = 0$

state → maximum entropy.

but

- $f_{\text{Max}} [n(x), T(x), V(x)]$ does not satisfy Boltzmann eqn. ⇒ $dF \neq 0$.

i.e. $\nabla \cdot \mathbf{D} f = c c f$

⇒ $F = f_{\text{Max}} + dF$

Why? → gradients in thermodynamic quantities ⇒ system is not in maximum entropy state i.e. $dF \neq 0$

- so $dF \sim \nabla C$ ⇒ relaxation to maximum entropy state will occur by collisions / transport

- can describe relaxation macroscopically, i.e.

$$\underbrace{\Pi_{\alpha, \beta}}_{\text{flux}} = -\rho D \underbrace{\frac{\partial V_{\beta}}{\partial x_{\alpha}}}_{\text{force}} \quad \frac{\partial p v}{\partial t} = -\nabla \cdot \underline{\underline{\Pi}}$$

$$-\frac{\partial V_{\beta}}{\partial x_{\alpha}} \Pi_{\alpha, \beta} = \rho D \left(\frac{\partial V_{\beta}}{\partial x_{\alpha}} \right)^2 \quad \int \dot{E}_v = \int \underline{\underline{\Pi}} \cdot \underline{\underline{\nabla}}$$

$$\boxed{\frac{dS}{dt} = \frac{\rho D}{T} \left(\frac{\partial V_{\beta}}{\partial x_{\alpha}} \right)^2}$$

- entropy production due transport
- induced relaxation

Note time scales:

i.) to form local Maxwellian, H-thm. $\Rightarrow \tau_{coll} \sim \nu^{-1}$

ii.) to form global ~~maximum~~ entropy state:

$$\frac{1}{\tau_{relax}} \sim \nu / L^2 \sim \nu \frac{L_{mix}^2}{L^2}$$

$$L_{\nu}^{-1} = \frac{\nu}{L} \frac{\partial V}{\partial x}$$

$$\tau_{relax} \sim \left(L_V / l_{MFP} \right)^2 \tau_{coll}$$

⇒ entropy production / relaxation is multiple time scale process!

More generally, can write:

$$J_i = - \sum_{j=1}^n \alpha_{ij} X_j^*$$

$\underbrace{\hspace{10em}}_{\text{kinetic coefficient}}$

$\xrightarrow{X_j^*}$ driving force

$$\frac{dS}{dt} = \psi = \text{"dissipation function"}$$

$$\Rightarrow \frac{dS}{dt} = \sum_{i=1}^n \sum_{j=1}^n \alpha_{ij} X_i X_j$$

i.e. $\frac{dS}{dt} = - X_j J_i$

so, for 2x2:

$$\frac{dS}{dt} = \sum_{i=1}^2 \sum_{j=1}^2 \alpha_{ij} X_i X_j = \alpha_{11} X_1^2 + (\alpha_{12} + \alpha_{21}) X_1 X_2 + \alpha_{22} X_2^2$$

clearly need:

$$\begin{array}{l} \alpha_{1,1} \geq 0 \\ \alpha_{2,2} \geq 0 \end{array} \rightarrow \text{i.e. diffusion down gradient}$$

$$\text{and } \alpha_{1,1} \alpha_{2,2} - \frac{1}{4} (\alpha_{1,2} + \alpha_{2,1})^2 \geq 0.$$

(i.e. decou \rightarrow drag.)

N.B. off-diagonals $\neq 0$!

i.e. can ∇T drive a density flux?

$$\Gamma = \int d^3v \mathbf{v} \delta f$$

$$\delta f = -\frac{1}{T} \mathbf{v} \cdot \nabla f_0$$

$$\Rightarrow \Gamma = \int d^3v \mathbf{v} \left(-\frac{1}{T} \mathbf{v} \cdot \nabla \left(\frac{n_0}{(2\pi)^3} \exp\left[-\frac{mV^2}{2T(x)}\right] \right) \right)$$

clearly can get contribution to Γ_x .
 \rightarrow Thermal diffusion.

Message: Gradient on distribution function is the key! --- but integration symmetric matter.