

PHYSICS 210A : STATISTICAL PHYSICS
HW ASSIGNMENT #4 SOLUTIONS

(1) $\nu = 8$ moles of a diatomic ideal gas are subjected to a cyclic quasistatic process, the thermodynamic path for which is an ellipse in the (V, p) plane. The center of the ellipse lies at $(V_0, p_0) = (0.25 \text{ m}^3, 1.0 \text{ bar})$. The semimajor and semiminor axes of the ellipse are $\Delta V = 0.10 \text{ m}^3$ and $\Delta p = 0.20 \text{ bar}$.

- (a) What is the temperature at $(V, p) = (V_0 + \Delta V, p_0)$?
- (b) Compute the net work per cycle done by the gas.
- (c) Compute the internal energy difference $E(V_0 - \Delta V, p_0) - E(V_0, p_0 - \Delta p)$.
- (d) Compute the heat Q absorbed by the gas along the upper half of the cycle.

Solution :

(a) The temperature is $T = pV/\nu R$. With $V = V_0 + \Delta V = 0.35 \text{ m}^3$ and $p = p_0 = 1.0 \text{ bar}$, we have

$$T = \frac{(10^5 \text{ Pa})(0.35 \text{ m}^3)}{(8 \text{ mol})(8.31 \text{ J/mol K})} = 530 \text{ K} .$$

(b) The area of an ellipse is π times the product of the semimajor axis lengths.

$$\oint p dV = \pi (\Delta p)(\Delta V) = \pi (0.20 \times 10^6 \text{ bar}) (0.10 \text{ m}^3) = 6.3 \text{ kJ} .$$

(c) For a diatomic ideal gas, $E = \frac{5}{2}pV$. Thus,

$$\Delta E = \frac{5}{2}(V_0 \Delta p - p_0 \Delta V) = \frac{5}{2}(-0.05 \times 10^5 \text{ J}) = -13 \text{ kJ} .$$

(d) We have $Q = \Delta E + W$, with

$$W = 2 p_0 \Delta V + \frac{\pi}{2}(\Delta p)(\Delta V) = 23 \text{ kJ} ,$$

which is the total area under the top half of the ellipse. The difference in energy is given by $\Delta E = \frac{5}{2} p_0 \cdot 2\Delta V = 5 p_0 \Delta V$, so

$$Q = \Delta E + W = 7 p_0 \Delta V + \frac{\pi}{2}(\Delta p)(\Delta V) = 73 \text{ kJ} .$$

(2) Consider a thermodynamic system for which $E(S, V, N) = aS^4/NV^2$.

- (a) Find the equation of state $p = p(T, V, N)$.
- (b) Find the equation of state $\mu = \mu(T, p)$.
- (c) ν moles of this substance are taken through a Joule-Brayton cycle. The upper isobar lies at $p = p_2$ and extends from volume V_A to V_B . The lower isobar lies at $p = p_1$. Find the volumes V_C and V_D .
- (d) Find the work done per cycle W_{cyc} , the heat Q_{AB} , and the cycle efficiency.

Solution :

(a) We can find

$$p = - \left(\frac{\partial E}{\partial V} \right)_{S,N} = \frac{2aS^4}{NV^3} \quad , \quad T = \left(\frac{\partial E}{\partial S} \right)_{V,N} = \frac{4aS^3}{NV^2} \quad , \quad \mu = \left(\frac{\partial E}{\partial N} \right)_{S,V} = - \frac{aS^4}{N^2V^2} \quad ,$$

but we need to eliminate the inconvenient variable S from these equations. To do this, we construct the ratio p^3/T^4 , in which the S factors manifestly cancel. One then finds $32ap^3V = NT^4$, i.e.

$$p(T, V, N) = (32a)^{-1/3} \left(\frac{N}{V} \right)^{1/3} T^{4/3} .$$

This means, for example, that the equation for an isotherm (at fixed N) is $pV^{1/3} = \text{const.}$, in contrast to the result for the ideal gas isotherm, $pV = \text{const.}$ Note also that p , being intensive, must be expressible as $p(T, V/N)$, which it is.

(b) To obtain $\mu(T, p)$, note that $2N\mu = -pV$, and from our result for $p(T, V/N)$ we have $V/N = T^4/32ap^3$. Thus,

$$\mu(T, p) = - \frac{T^4}{64ap^2} .$$

(c) The equilibrium adiabatic equation of state for this system is $dS = 0$. From (a), we see that at fixed N this means $pV^3 = \text{const.}$, so we must have $p_2V_B^3 = p_1V_C^3$ and $p_2V_A^3 = p_1V_D^3$. Hence

$$V_C = V_B \cdot (p_2/p_1)^{1/3} \quad , \quad V_D = V_A \cdot (p_2/p_1)^{1/3} .$$

(a) From part (a), the energy for our system is $E = \frac{1}{2}pV$. Along the upper (p_2) isochore,

$$W_{AB} = \int_A^B dV p_2 = p_2(V_B - V_A) \quad , \quad \Delta E_{AB} = E_B - E_A = \frac{1}{2}p_2(V_B - V_A) \quad ,$$

hence

$$Q_{AB} = \Delta E_{AB} + W_{AB} = \frac{3}{2}p_2(V_B - V_A) .$$

The work along the lower (p_1) isochore is

$$W_{CD} = p_1(V_D - V_C) = p_2(V_A - V_B) \left(\frac{p_1}{p_2}\right)^{2/3}.$$

Along the BC adiabat,

$$W_{BC} = \int_B^C p dV = p_2 V_B^3 \int_{V_B}^{V_C} \frac{dV}{V^3} = \frac{1}{2} p_2 V_B \left(1 - \frac{V_B^2}{V_C^2}\right) = \frac{1}{2} p_2 V_B \left[1 - \left(\frac{p_1}{p_2}\right)^{2/3}\right].$$

Similarly,

$$W_{DA} = \int_D^A p dV = p_2 V_A^3 \int_{V_D}^{V_A} \frac{dV}{V^3} = \frac{1}{2} p_2 V_A \left(\frac{V_A^2}{V_D^2} - 1\right) = \frac{1}{2} p_2 V_A \left[\left(\frac{p_1}{p_2}\right)^{2/3} - 1\right].$$

Adding up all the individual works, we get

$$\begin{aligned} W_{\text{cyc}} &= W_{AB} + W_{BC} + W_{CD} + W_{DA} \\ &= \frac{3}{2} p_2 (V_B - V_A) \left[1 - \left(\frac{p_1}{p_2}\right)^{2/3}\right]. \end{aligned}$$

Dividing by Q_{AB} , we obtain the efficiency,

$$\eta = \frac{W_{\text{cyc}}}{Q_{AB}} = 1 - \left(\frac{p_1}{p_2}\right)^{2/3}.$$

(3) A diatomic gas obeys the equation of state

$$p = \frac{RT}{v-b} - \frac{a}{v^2} + \frac{cRT}{v^3},$$

where a , b , and c are constants.

- Find the adiabatic equation of state relating temperature T and molar volume v .
- What is the internal energy per mole, $\varepsilon(T, v)$?
- What is the Helmholtz free energy per mole, $f(T, v)$?

Solution :

(a) Let ε be the molar internal energy and v the molar volume. We have already shown

$$\left(\frac{\partial \varepsilon}{\partial v}\right)_T = T \left(\frac{\partial p}{\partial T}\right)_v - p.$$

Thus, for our system,

$$\left(\frac{\partial \varepsilon}{\partial v}\right)_T = \frac{a}{v^2} \Rightarrow \varepsilon(T, v) = \frac{5}{2}RT - \frac{a}{v},$$

where the first term is the result for the rarefied limit $v \rightarrow \infty$, where the gas presumably becomes ideal. Now if $s = S/\nu$ is the molar entropy ($\nu = N/N_A$ is the number of moles), then

$$T ds = d\varepsilon + p dv = \frac{5}{2}R dT + RT \frac{dv}{v-b} + cRT \frac{dv}{v^3}.$$

Dividing by T and then integrating, we have

$$s(T, v) = R \ln \left[T^{5/2} (v-b) e^{-c/2v^2} \right] + \text{const.}$$

Thus, the equation of the adiabat is

$$T^{5/2} (v-b) e^{-c/2v^2} = \text{const.}$$

(b) We have already obtained the result

$$\varepsilon(T, v) = \frac{5}{2}RT - \frac{a}{v}.$$

(c) From $f = \varepsilon - Ts$, where $f = F/\nu$ is the Helmholtz free energy per mole, we have

$$f(T, v) = \frac{5}{2}RT - \frac{a}{v} - \frac{5}{2}RT \ln \left(\frac{bRT}{a} \right) - RT \ln \left(\frac{v-b}{b} \right) + \frac{cRT}{2v^2} - Ts_0.$$

Here we have inserted constants with the proper dimensions in order to render our expression for f with the appropriate dimensions. Thus, the constant s_0 has dimensions of J/mol · K, the same as the gas constant R . Since c/b^2 is dimensionless, there is more than one way to do this. Any resulting differences will show up in a different expression for s_0 .

(4) Consider the thermodynamics of a solid in equilibrium with a vapor at temperature T and pressure p , but separated by a quasi-liquid layer of thickness d . Let the number density of the liquid be n_ℓ . The Gibbs free energy per unit area of the quasi-liquid layer is taken as

$$g_{qll}(T, p) = n_\ell \mu_\ell(T, p) d + \gamma(d),$$

where $\gamma(d)$ is an effective surface tension which interpolates between $\gamma(0) = \gamma_{sv}$ and $\gamma(\infty) = \gamma_{sl} + \gamma_{lv}$. The phenomenon of premelting requires $\gamma(0) > \gamma(\infty)$.

(a) Show that $\mu_{qll}(T, p) = \mu_\ell(T, p) + n_\ell^{-1} \gamma'(d) = \mu_s(T, p)$.

(b) Expand T relative to some point (T_m, p) along the melting curve to lowest order in $T - T_m$. Show $\Delta\mu(T, p) \equiv \mu_s(T, p) - \mu_\ell(T, p) = \ell_m(T - T_m)/T_m$, where ℓ_m is the latent heat of melting.

(c) Assume

$$\gamma(d) = \gamma_{sv} + (\gamma_{sl} + \gamma_{lv} - \gamma_{sv}) \cdot \frac{d^2}{d^2 + \sigma^2},$$

where σ is a molecular length scale. Assuming $d \gg \sigma$, find the dependence of the thickness d of the quasi-liquid layer on the reduced temperature $t \equiv (T_m - T)/T_m$.

Solution :

(a) The chemical potentials of a particle in the solid and the quasi-liquid layers must be the same. Since we use d for thickness, I will here use δ for differential. The Gibbs free energy of the quasi-liquid layer is $G_{qll}(d) = Ag_{qll}(d)$, where A is the total surface area. The number of particles in the quasi-liquid layer is $N_{qll} = An_{qll}d$. Thus, the chemical potential is then

$$\mu_{qll} = \frac{\delta G_{qll}}{\delta N_{qll}} = \mu_\ell + n_\ell^{-1} \gamma'(d).$$

(b) Expanding to first order, with $\Delta\mu = \mu_s - \mu_\ell$, we have

$$\Delta\mu(T, p) = \left(\frac{\partial \Delta\mu}{\partial T} \right)_p (T - T_m) = \frac{\ell_m}{T_m} (T - T_m),$$

where ℓ_m is the latent heat of melting per molecule. This results in the desired expression $\Delta\mu(T, p) = \ell_m(T - T_m)/T_m$.

For a more rigorous derivation, expand to first order in both ΔT and Δp :

$$\begin{aligned} \Delta\mu(T, p) &= \left(\frac{\partial \Delta\mu}{\partial T} \right)_p (T - T_m) + \left(\frac{\partial \Delta\mu}{\partial p} \right)_T (p - p_m) + \dots \\ &= \frac{\ell_m}{T_m} (T - T_m) - \left(\frac{1}{n_\ell} - \frac{1}{n_s} \right) (p - p_m) + \dots \end{aligned}$$

The pressure shift can now be expressed in terms of the temperature shift by examining the slopes of the sublimation and melting lines, via the Clapeyron equation. This results in $\Delta\mu(T, p) = \kappa_v \ell_m(T - T_m)/T_m$, with

$$\kappa_v = 1 - \frac{(dp/dT)_{\text{subl}}}{(dp/dT)_{\text{melt}}}.$$

For water, $\kappa_v \approx 1$ and the correction is negligible.

(c) We now set

$$\Delta\mu = \frac{1}{n_\ell} \frac{\partial \gamma}{\partial d} = \frac{\gamma_{sl} + \gamma_{lv} - \gamma_{sv}}{n_\ell} \cdot \frac{2\sigma^2 d}{(\sigma^2 + d^2)^2} = \frac{\kappa_v \ell_m \Delta T}{T_m}.$$

For $d \gg \sigma$, we have

$$d(t) = \left(-\frac{2\sigma^2(\gamma_{sl} + \gamma_{lv} - \gamma_{sv})}{\ell_m n_\ell} \right)^{1/3} t^{-1/3},$$

where $t \equiv (T - T_m)/T_m$.